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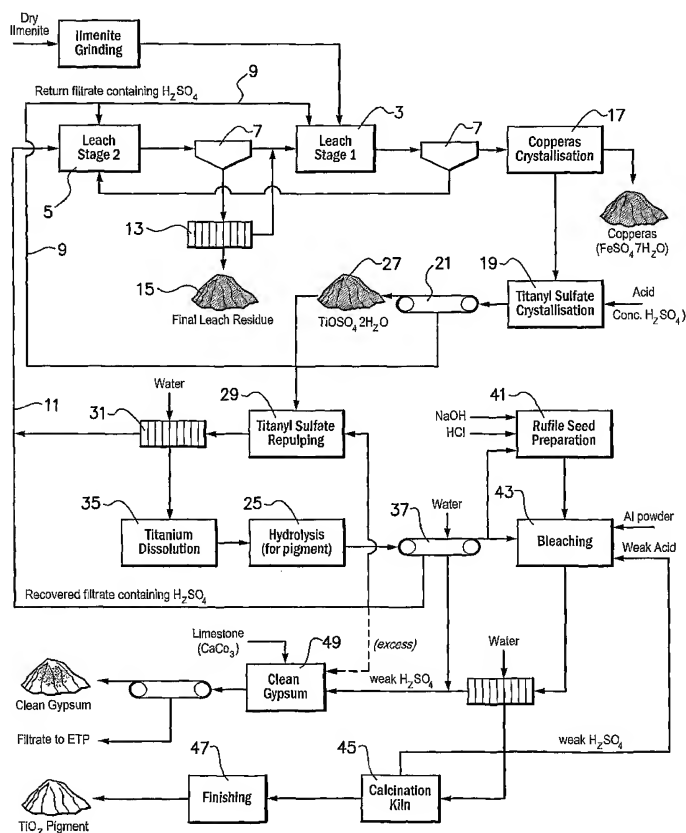
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[Continued on next page]

(54) Title: TITANIUM INTERMEDIATE PROCESSING



(57) Abstract: A sulfate process for producing titania from a titaniferous material as disclosed. The process is characterized by particular steps of separating precipitated titanyl sulfate from solution and subsequently treating the precipitated material prior to hydrolysis.



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TITANIUM INTERMEDIATE PROCESSING

The present invention relates to a process for producing titania from a titaniferous material.

The term "titaniferous" material is understood herein to mean any titanium-containing material, including by way of example ores, ore concentrates, and titaniferous slags.

The present invention relates particularly to the sulfate process for producing titania from titaniferous material.

International application PCT/AU2004/001421 in the name of the applicant describes an invention of a sulfate process made by the applicant. The disclosure in the International application is incorporated herein by cross-reference.

In general terms, the present invention provides a sulfate process for producing titania from a titaniferous material (such as ilmenite) of the type which includes the steps of:

(a) leaching the solid titaniferous material with a leach solution containing sulfuric acid and forming a process solution that includes an acidic solution of titanyl sulfate (TiOSO_4) and iron sulfate (FeSO_4);

(b) separating the process solution and a residual solid phase from the leach step (a);

(c) precipitating titanyl sulfate from the process solution from step (b);

(d) separating the precipitated titanyl sulfate

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from the process solution;

(e) treating the precipitated titanyl sulfate and producing a solution containing titanyl sulfate;

5

(f) hydrolysing the titanyl sulfate in the solution and forming a solid phase containing hydrated titanium oxides and a liquid phase;

10

(g) separating the solid phase containing hydrated titanium oxides and the liquid phase;

(h) calcining the solid phase from step (g) and forming titania; and

15

(i) removing iron sulfate from the process solution from step (b) and/or the depleted process solution from step (d).

20

The term "hydrated titanium oxides" is understood herein to include, by way of example, compounds that have the formula $\text{TiO}_2 \cdot 2\text{H}_2\text{O}$ and $\text{TiO}_2 \cdot \text{H}_2\text{O}$.

25

In addition, the term "hydrated titanium oxides" is understood herein to include compounds that are described in technical literature as titanium hydroxide ($\text{Ti}(\text{OH})_4$).

30

It is also noted at this point that acid concentrations mentioned hereinafter are understood herein as being determined by titration of an oxalate buffered solution sample with sodium hydroxide solution to an end point of pH 7.

35

It is also noted at this point that concentrations of metals mentioned hereinafter are understood herein as being determined by ICP (all metals)

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or by titration (in the cases of Ti and Fe - ferrous and ferric).

As is indicated in the above-mentioned
5 International application, US patent 3,760,058 in the name Langmesser et al (assigned to Farbenfabriken Bayer AK) discloses a part of the above-described process.

10 The reference herein to the Bayer US patent is not to be taken as an indication that the disclosure in the patent is part of the common general knowledge of persons skilled in the field of the invention.

15 Preferably the process includes supplying the separated process solution from step (d) and/or the separated liquid phase from step (g) to leach step (a).

20 The applicant has carried out further research work on the process since the priority date of 17 October 2003 of the International application and has identified a number of features that are not disclosed in the above-mentioned International application that are important, separately and in combination, in order to operate the process effectively and that form the basis of the present
25 invention.

The present invention is based on features of steps (d) and (e) of separating precipitated titanyl sulfate from process solution and subsequently treating
30 the precipitated material prior to hydrolysis that are described hereinafter that were identified in the further research work.

35 Other features of the above-described process that were identified in the further research work are described in the specification lodged with Australian provisional application 2005901749 in the name of the

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applicant and the disclosure in this specification is incorporated herein by cross-reference.

In the above-mentioned research work the applicant has found that it is preferable to separate the precipitated titanyl sulfate from the process solution from step (c) using a filter, such as a pressure filter, for example a pressure belt filter, which forms a filter cake and a filtrate.

In addition, the applicant has found that the filter cake, which contains solid titanyl sulfate and retained high acidity, typically 400-700 g/L, process solution, is a stable solid intermediate product that can be stored indefinitely and used as required.

Thus, the filtration achieved by the filter, which separates the solids from a substantial part of the process solution, provides a convenient circuit break for the process that makes it possible to operate the preceding and following steps in the process as separate unit operations.

The filter cake may be washed with fresh acid and/or recycled acid, for example from the hydrolysis step (f) described hereinafter, to displace entrained process solution containing impurities and thereby improve the purity of the subsequently formed high strength Ti solution for the hydrolysis step.

The filtrate from the filter typically contains 700 g/L sulfuric acid (50% w/v), 10 g/L titanium and 40 g/L iron in solution and is supplied to the leach step.

A substantial proportion, typically 80% by weight, of the filter cake is retained process liquor. The applicant has found that it is difficult to remove the

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retained process liquor from the filter cake after the filter cake has been removed from the filter by a straight washing step.

5 In particular, the applicant has found that it is preferable to re-pulp the filter cake and form an acidic slurry of titanyl sulfate and thereafter filter the slurry and wash the filter cake.

10 The applicant has also found that it is preferable to re-pulp the filter cake with an acidic solution in order to retain high acidity in the resultant slurry and so as to form an acidic slurry that has a low solids loading, typically less than 10% by weight, for
15 materials handling reasons, as described above. The slurry formed under these conditions has a sufficiently fluid consistency that it may be handled using conventional and commonly available process equipment.

20 Preferably the acidity of the acidic solution is at least 300 g/L.

 Preferably the acidity of the acidic solution is of the order of 400 g/L.

25 Preferably the acidic solution includes the liquid phase recovered from the hydrolysis step (f) and/or recycled re-pulp acid.

30 Preferably the re-pulping is under agitated conditions.

 The acidic slurry is filtered using a filter, such as a pressure filter, for example a pressure belt
35 filter, to form a filter cake of titanyl sulfate and a filtrate. In one embodiment the filter cake is washed using the liquid phase recovered from hydrolysis step (f).

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Furthermore, the applicant has found that it is preferable to wash the acidic filter cake of titanyl sulfate with water and reduce the acidity of the liquid component of the filter cake to be less than 200 g/L acid. The applicant has found that the solids in the filter cake become unstable at acid concentrations of less than 200 g/L and thereafter dissolve in step (e). Thus reduction in acid concentration by washing with water is important to achieve subsequent dissolution of titanyl sulfate in step (e).

Furthermore, the applicant has also found that it is preferable to minimise the amount of water that is retained with the precipitated titanyl sulfate. Minimising retained water is important in order to maximise the titanium concentration in the subsequently dissolved process solution produced in step (e), preferably to concentrations of at least 150 g/L, more preferably at least 200 g/L titanium.

In order to minimise the retained water, preferably step (d) includes washing the acidic filter cake of titanyl sulfate with water under pressure filtration conditions, such as on a belt pressure filter, and removing as much liquid as possible from the titanyl sulfate.

Alternatively, the titanyl sulfate may be concentrated by evaporation or other suitable options for removing retained water.

Furthermore, the applicant has found that it is preferable that step (e) includes transferring the washed filter cake to a stirred tank and allowing the cake to dissolve to a process solution containing a high concentration of titanium, preferably at least 150 g/L,

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more preferably at least 200 g/L titanium.

The applicant has found that it is preferable to heat the washed filter cake in the stirred tank, preferably to a temperature of the order of 60° C in order to speed up the dissolution process.

The dissolution process may be carried out on a batch or a continuous basis.

In addition, high strength process solution ("rich liquor") produced in the dissolution process may be recycled to the stirred tank to improve agitation and/or handling of the slurry as dissolution is proceeding.

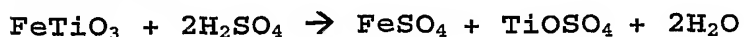
The applicant has also found that steps (d) and (e) may be carried out successively, with no stockpiling of an intermediate solid product.

Specifically, steps (d) and (e) may include separating the precipitated titanyl sulfate from the process solution from step (c), for example on a filter and producing a filter cake, and thereafter directly washing the filter cake with the liquid phase from step (f) and/or water, for example while the filter cake is on the filter.

Steps (d) and (e) may include air blowing and/or squeezing the filter cake and removing additional liquid from the filter cake and producing a high Ti concentration in the subsequent dissolved liquor.

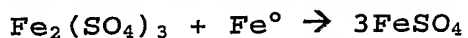
The process of the present invention includes the following typical reactions.

Leaching:

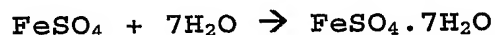


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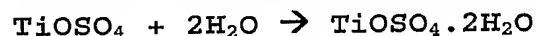
Ferric reduction:



5 Ferrous sulfate crystallisation:



Titanyl sulfate precipitation:

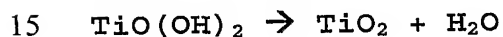


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Hydrolysis:



Calcination:



The applicant has carried out experimental work on a laboratory scale and a pilot plant scale in relation to the above-described process.

20

The improved sulfate process of the present invention is now described further by way of example only with reference to the accompanying flow sheet.

25

The flowsheet includes the following main steps:

(a) leach;

(b) ferrous sulfate crystallisation;

30

(c) titanyl sulfate crystallisation;

(d) titanium dissolution;

35

(e) hydrolysis for pigment;

(f) rutile seed preparation;

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(g) bleaching,

(h) calcination; and

(i) finishing.

Each of the above steps is described hereinafter in turn.

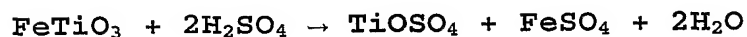
(a) Leach Step

The leach step includes two leach stages 1 and 2 carried out in separate tanks 3, 5.

Each leach stage is carried out in a single tank 3, 5 as indicated in the flowsheet or in multiple tanks (not shown) arranged in series.

The leach stages 1 and 2 may be a fully counter-current or may be co-current with fresh return filtrate and/or wash filtrates being added to both leach stages.

The chemistry of the leach step is:



Leaching is carried out at a controlled acidity of 450 g/L (± 25 g/L) H_2SO_4 in each stage. Under these conditions about 80% leaching takes place in two leach stages, each of about 12 hours residence time.

The leaching temperature is typically 110° C in each stage, which is less than the solution boiling point. The temperature is not controlled, but sufficient heat is generated during leaching to keep the slurry at about 110° C. Some top-up steam may be required for start up.

- 10 -

One option is to use scrap iron addition into the leach tanks 3, 5. This has been found to increase leach kinetics significantly. Some reductant is required to
5 convert ferric sulfate to ferrous sulfate to allow all iron to exit in the form of FeSO_4 crystals.

The leach tanks 3, 5 are simple stirred tanks, each of which operates with an overflow to a thickener 7.
10 Fibre-reinforced plastic (FRP) is suitable for wetted parts. Other suitable materials are acid bricks and tiles.

The leach tanks 3, 5 are operated with gentle
15 stirring so that the residence time of solids in the tanks is longer than the residence time of liquor in the tanks.

The leach slurries discharged from the tanks 3, 5 are thickened in conventional thickeners 7. The settling
20 rate is high for partly reacted ilmenite. Flocculation is possible. Underflow densities exceeding 60% are feasible, but lower solids loadings may be required to ensure pumpability.

The solids loading in the leach step is
25 controlled to give a process solution of about 40 g/L Ti, 90-100 g/L Fe and 400-450 g/L acid that leaves the leach step as overflow from the downstream thickener 7. These are the preferred concentrations of Fe and Ti without
30 having ferrous sulfate or titanyl sulfate crystallise out prematurely.

Ilmenite is added dry to the first leach tank 3.

35 To control the acidity to 450 g/L (± 25 g/L) return filtrate from a titanyl sulfate crystallisation step 19 discussed hereinafter is supplied via line 9 to the

- 11 -

tanks 3, 5 and/or additional sulfuric acid is metered into the tanks 3, 5. In situations where there are multiple tanks 3, 5 in each stage, most of the acid is added to the first two tanks 3, 5 in each stage. In practice, the acidity in later tanks may be uncontrolled.

Thickener underflow from the thickener 7 of the first leach stage is pumped to the leach tank 5 of the second leach stage.

Some recycled acid at about 350 g/L (± 25 g/L) H_2SO_4 , which is a filtrate from a filtration step 37 downstream of a hydrolysis step 25 described hereinafter, is also pumped via line 11 to the leach tank 5.

Titanyl sulfate crystallisation filtrate produced in a filtration step 31 described hereinafter is also added via line 11 to the second tank 5 to maintain the acidity at 450 g/L (± 25 g/L).

Leaching is about 50-60% in the first stage rising to about 80% overall by the end of the second stage. Higher extractions are feasible with further leaching.

The second stage leach slurry that is discharged from the leach tank 5 is thickened in the thickener 7.

In a full counter-current operation the second stage overflow from the thickener 7 is pumped to the first stage leach tank 3. In a co-current circuit the solids loading is higher in both stages so that the target of 40 g/L Ti is reached in the final process solution.

Second stage leach residue is filtered via filter 13 and the resultant filter cake is suspended in recycled water. Limestone and lime are added to raise the pH to 7-

- 12 -

8, and the slurry is pumped to tailings 15.

The process solution contained in the (unwashed) filter cake that is supplied to tailings 15 represents the major outlet for a number of minor elements, such as Cr and Zn.

Low acidity in the leach stages can cause the premature hydrolysis and precipitation of $\text{TiO}(\text{OH})_2$. Typically this becomes significant below about 425 g/L H_2SO_4 . Above 450 g/L H_2SO_4 it is likewise possible to prematurely crystallise out titanyl sulfate dihydrate, $\text{TiOSO}_4 \cdot 2\text{H}_2\text{O}$.

15 (b) Ferrous Sulfate Crystallisation Step

Almost all iron in solution eventually leaves the circuit as green crystals of ferrous sulfate $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ in a ferrous sulfate crystallization step 17.

20

Significant water is also rejected from the process in the ferrous sulfate, also known as "copperas". This allows recovery and recycling of medium strength acid from the hydrolysis step, leading to a much lower overall acid consumption per tonne of TiO_2 product.

25

In the ferrous sulfate crystallization step 17, hot process solution discharged as the overflow from the downstream thickener 7 of the leach step is firstly cooled to about 60°C in a heat exchanger (not shown) by heat exchange with process solution that has been discharged from a downstream crystallization tank (not shown).

30

The cooled pregnant process solution is then evaporatively cooled to about 20°C. This causes ferrous sulfate to crystallise out in the tank. The cooled process solution at this stage contains about 40 g/L Fe

35

- 13 -

and 55 g/L Ti. The Ti concentration rises due to the lower volume of the cooled process solution.

Removal of water by evaporation may be included
5 to give a further water credit, allowing recovery of more weak acid.

The ferrous sulfate crystals may be separated from the process solution by a conventional centrifuge
10 (not shown) or by a belt filter (not shown).

Some washing may be possible, but the high solubility of the crystals means that washing should be minimised if possible.
15

The ferrous sulfate may be sold directly or converted to another saleable product.

Although 40g/L Fe remains in solution, the iron
20 is recirculated and eventually returns to the ferrous sulfate crystallization step 17. The ferrous sulfate crystals therefore are essentially the only point of exit for iron from the circuit.

25 Mn, Al and Mg are minor elements which exit the circuit primarily with the ferrous sulfate crystals.

Finally, the cold process solution that is discharged from the ferrous sulfate crystallization step
30 17 is partially reheated by cross flow heat exchanging against incoming hot process solution supplied to the step 17.

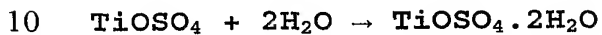
(c) Titanyl Sulfate Precipitation Step
35

Fresh 98% sulfuric acid that is required for leaching ilmenite is not added in the leach stages of the

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leach step. Instead, the acid is added in the titanyl sulfate precipitation step, generally identified by the numeral 19.

5 The acid causes titanium to precipitate out of the process solution as titanyl sulfate dihydrate, $\text{TiOSO}_4 \cdot 2\text{H}_2\text{O}$, and form a slurry in accordance with the following reaction:



 The actual mechanism of precipitation is not clear.

15 The preferred operating temperature in the titanyl sulfate precipitation step is 110°C . Precipitation is very slow at less than 90°C .

20 Precipitation is self seeding - the kinetics of crystallisation are accelerated by the presence of the product crystals.

25 The solids have a long needle-like shape (typically $1\mu\text{m}$ width by $100\mu\text{m}$ long). The needle-like morphology causes significant rheology problems in the titanyl sulfate precipitation step. Quite low solids loadings can result in thick porridge-like slurries which resist pumping and agitation.

30 In one particular embodiment the precipitation tank (or one or more than one of the precipitation tanks in situations where there are multiple tanks) has an upstanding draft tube that has an upper inlet and a lower outlet and the draft tube is located to divide the tank
35 into an outer chamber and a central cylindrical chamber. The assembly also includes an impeller to help circulation of the slurry. The slurry flows through the draft tube

- 15 -

and the outer chamber in the tank.

To keep the slurry in a fluid state a recycle of filtrate may be used.

5

The solids in the slurry that is discharged from the precipitation tank or tanks are separated from the slurry by filtration. Filtration may be by a belt filter 21 shown in the flowsheet. However, maintaining the temperature of the filtrate probably requires pressure filtration.

10

Some washing of the solids in the filter cake on the filter 21 by recycled acid from the hydrolysis step described hereinafter may be carried out as this improves purity of the high strength Ti solution going to hydrolysis.

15

The acid washed $\text{TiOSO}_4 \cdot 2\text{H}_2\text{O}$ filter cake is a stable solid product and offers a convenient breakpoint in the flowsheet. The filter cake may be stock-piled as indicated by the numeral 27. Temporary storage of the acid washed crystals offers useful buffer capacity, and makes the process more robust.

20

25

The filtrate contains about 700 g/L H_2SO_4 (roughly 50% w/v) plus 10 g/L Ti and 40 g/L Fe. Some is recycled to the titanyl sulfate precipitation stage tank 19. The rest is sent to the leach stages via line 9, where it is used to control the acidity to 450 g/L H_2SO_4 in the leach slurry.

30

Thickening before filtration is not used due to the needle-like solids, which do not compact readily under gravity.

35

(d) Titanium Dissolution

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The acid washed filter cake from the stockpile 27 is re-pulped in a 30% H_2SO_4 solution in a re-pulping step 29 and is then is pumped to a filter 31. The resultant
5 slurry has an acid concentration of the order of 400 g/L.

The filter cake on the filter 31 may be washed with hydrolysis filtrate to remove remaining entrained leach liquor.

10

Finally, a carefully controlled water wash is used to displace all the remaining acid in the filter cake on the filter 31. Reducing the acid concentration to below 200 g/L destabilises the solids, leading to ultimate
15 dissolution of the solids. Cake squeezing and/or air blowing is then used to control the moisture content of the cake. About 5 g/L Ti reports to the wash filtrate, which is recycled via line 11 to the leach stages.

20

As described above, these washing steps may be applied to the initial filtration step to eliminate the need to re-pulp and re-filter the solids. However, in doing so the ability to store an intermediate filter cake is lost and the process is less robust.

25

The water washed filter cake discharged from the filter 31 is added to a stirred tank 35. Over a period of about 2 hours at 60°C the cake dissolves into a high strength Ti solution. Lower temperatures can also be
30 used, although the dissolution time may be longer than 2 hours.

The target concentration is 150 g/L Ti (= 250 g/L "TiO₂"). Concentrations exceeding 200 g/L Ti have been
35 produced in laboratory and pilot plant work. However, 150 g/L or above is suitable for conventional pigment hydrolysis.

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The dissolution process preferably requires less than 100 g/L acid in the solution contained within the filter cake to ensure that the process goes to completion. If most or all acid is washed out the free acid content of the high strength solution is quite low. In pigment industry terms the acid to titania (A/T) ratio is usually about 1.3 (the theoretical minimum is 1.225 at zero acidity).

The product high strength solution produced in the stirred tank 35 is filtered through a filter cartridge (not shown) to remove siliceous and other fine particulate matter.

Unlike normal metal sulfates, the $\text{TiOSO}_4 \cdot 2\text{H}_2\text{O}$ in the filter cake does not immediately dissolve in water. Also its solubility in $>20\%$ H_2SO_4 is quite low. This suggests the dissolution process is not strictly dissolution. The remarkable solubility of Ti at low acidity (>200 g/L Ti) compared to 20% H_2SO_4 (~ 5 g/L Ti) favours this view.

(e) Hydrolysis Step

The high strength Ti process solution is suitable for all conventional pigment hydrolysis processes.

It also may be used for continuous or batch precipitation of coarse high purity $\text{TiO}(\text{OH})_2$.

The pigment hydrolysis processes are typically batch processes due to critical need to control particle size.

Feed solution to the pigment hydrolysis step is pretreated to generate about 2 g/L of Ti^{3+} in the solution

- 18 -

by conventional means. The Ti^{3+} protects against oxidation of any iron to Fe^{3+} , which coprecipitates with the Ti and imparts undesirable colour to the pigment.

5 The process solution is then adjusted with acid to an A/T ratio suitable for pigmentary hydrolysis, using either concentrated H_2SO_4 or preferably the hydrolysis filtrate. The A/T ratio is a key process parameter. A/T ratio is:

10
$$[\text{Free acid} + \text{bound acid in TiSO}_4] \div [\text{TiO}_2]$$

 All parameters are expressed in g/L.

15 In practice the [Free acid + bound acid in TiOSO_4] concentration is measured by a simple titration to pH 7 with sodium hydroxide solution, and the $[\text{TiO}_2]$ g/L is $\text{Ti g/L} \div 0.6$.

20 In one example of commercial practice, the hydrolysis is carried out by preheating a heel of water, typically 10-20% of the volume of feed solution, to about 96°C .

25 The process solution is also preheated to about 96°C and then is pumped across to the batch hydrolysis tank over a fixed time period.

30 The hydrolysis tank 25 is equipped with steam heating and a gate type rake stirrer, which operates at low rpm. Preferably the steam heating is indirect so that the filtrate is not diluted by condensate.

35 The initial few seconds of pumping cause the precipitation of very fine $\text{TiO}(\text{OH})_2$ particles, which cause a milky aspect for about 30 seconds, then appear to redissolve. In practice the fine particles are colloidal

- 19 -

nuclei which control the size of both the resulting precipitate and the crystal size in the calciner discharge. Control of this step is therefore key to preparing good pigment.

5

After all process solution is pumped across or dropped in from a header tank, the slurry temperature is carefully heated to the boiling point (typically at 1° C/minute).

10

The slurry is then boiled for about 5 hours, by which time the Ti remaining in solution has been lowered to about 5 g/L.

15

The slurry discharged from the hydrolysis tank 25 is filtered and washed with water on a belt filter 37 and produces a $\text{TiO}(\text{OH})_2$ filter cake and a filtrate.

20

There are no special requirements for filtration as the particle size has already been established. A range of filters are used across the industry. The particles naturally floc together and the filtration rate is fast enough that vacuum filtration may be used. The filter cake contains about 55% w/w of water.

25

The filtrate from the filter 37 contains 350-450 g/L H_2SO_4 . This is returned via line 11 to the leach step for slurrying ilmenite and/or first stage thickener underflow. The acid units thereby are used to leach ilmenite. Recycling this acid is limited by the overall circuit water balance, and is favoured by higher acidity (ie. a lower volume equates to the higher acidity). Any excess is sent to a clean gypsum plant 49.

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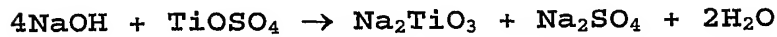
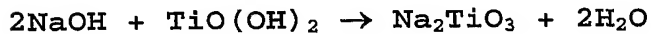
35 (f) Rutile Seed Preparation Step

In one example of commercial practice, rutile

- 20 -

seed is made in a rutile seed preparation step 41 by reacting some $\text{TiO}(\text{OH})_2$ filter cake discharged from the belt filter 37 with commercial 50% NaOH solution, for several hours at the boiling point (about 117°C):

5

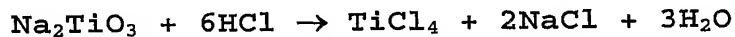


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The $\text{TiO}(\text{OH})_2$ filter cake contains about 4% S in the form of absorbed basic titanium sulfates. The resulting sodium titanate is filtered and washed well to completely remove sulfate. The washed cake is then mixed with a carefully controlled amount of commercial 35% HCl

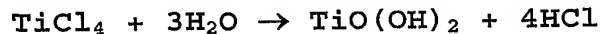
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to produce a solution of TiCl_4 ;



20

The solution is then boiled to generate ultrafine $\text{TiO}(\text{OH})_2$ particles:



25

The resulting slurry contains about 100 g/L TiO_2 in the rutile form. It may be used directly if the downstream flowsheet can tolerate Cl or it can be decantation washed to remove the NaCl.

(g) Bleaching Step

30

The $\text{Ti}(\text{OH})_2$ filter cake that is discharged from the belt filter 37 and is not used to make rutile seed is re-pulped with clean H_2SO_4 solution in a bleaching step 43. Al or Zn dust is added to reductively leach out

35

chromophores such as Fe, Cr, Mn and V, which otherwise would reduce the whiteness of the final pigment.

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The bleach step typically takes place at 80° C. The rutile seed slurry is added at this point in a carefully controlled amount (e.g. 4.0 ± 0.1 % w/w). The bleached slurry is filtered and washed.

5

The $\text{TiO}(\text{OH})_2$ filter cake, which has a sulfur content of about 2%, is mixed with a number of additives. These may be added as water solutions, or solids. The additives may include 0.2% K_2O as K_2SO_4 , 0.6% ZnO as ZnSO_4 and 0.3% P_2O_5 as H_3PO_4 .

10

The additives control development of the rutile crystals during calcination, such that the crystal size is $0.27 \pm 0.03 \mu\text{m}$, rutilisation is $98.5 \pm 0.5\%$, the crystals have a lenticular shape and are not sintered together.

15

In addition to the above-described steps, the process flowsheet also includes the steps of: calcination 45, finishing 47, and, if required, clean gypsum production 49. These steps are conventional steps.

20

Many modifications may be made to the process flowsheet described above without departing from the spirit and scope of the present invention.

25

By way of example, as an alternative to pigment production, the process is able to produce coarse high purity titania that can be used, for example, as a feedstock for electrochemical reduction to produce titanium metal and alloys. Hydrolysis may be carried out continuously in this option. Several simple stirred tanks may be used in a cascade arrangement. Hydrolysis may be carried out at boiling point using steam heating, preferably indirect. Seeding is carried out by recycling thickener underflow to the first tank. This allows the slurry residence time to be 8-12 hours and generates a particle size d_{50} of about 20 microns. Thickening gives a

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dense slurry of about 30% solids by weight, which may be vacuum filtered and washed. Bleaching may be carried out per the pigment process, if required. No rutile or chemical seeds are used. Calcination only requires a
5 temperature of the order of 900°C for about 1 hour.

The present invention is described further with reference to the following examples.

10 Within these examples where 'free H₂SO₄' has been referred to, this has been determined by titration of an oxalate buffered solution sample with sodium hydroxide solution to an end point of pH 7.

15 Example 1

 This example describes a first stage of batch leaching.

20 A solution (300L) containing 3.0 g/L Ti, 11.2 g/L Fe²⁺, 3.0 g/L Fe³⁺, and 716 g/L free H₂SO₄ was heated in a stirred, baffled vessel. Once the liquor had reached 110°C, 79.6 kg of ilmenite concentrate containing 25.9% FeO, 19.3% Fe₂O₃ and 50.4% TiO₂, which had previously been
25 ground in a ball mill to 80% less than 38 µm, was introduced into the reaction vessel. Six 10 mm diameter mild steel rods were suspended in the reactor such that about 200 mm of the rods extended below the solution level. The mixture was allowed to react at 110°C for 3
30 hours, after which the temperature was allowed to fall steadily to 80°C over the next 3 hours. The resulting slurry was filtered through a recessed plate filter and the cake was washed with fresh water. The filtrate contained 47 g/L Ti, 55 g/L Fe²⁺, 17 g/L Fe³⁺, 618 g/L free
35 H₂SO₄, and had a specific gravity of 1.637 g/cm³. The weight of the washed filter cake was 39kg with a moisture content of 16.9%. The washed filter cake was assayed on a

- 23 -

dry weight basis and was found to contain 15.3% FeO, 24.4% Fe₂O₃ and 48.7% TiO₂.

Based on the weights and compositions of the
5 ilmenites and cake, 60.6% of the TiO₂ in the ilmenite has dissolved during the leach process.

Example 2

10 This example describes a second stage of leaching using the first stage leach residue.

A solution (273 L) containing 3.6 g/L Ti, 6.1 g/L Fe²⁺, 2.4 g/L Fe³⁺, and 711 g/L free H₂SO₄ was heated in a
15 stirred, baffled vessel. Once the liquor had reached 110°C, 130 kg of wet cake prepared as described in Example 1, having a moisture content of 18.6% and containing 17.0% FeO, 22.7% Fe₂O₃ and 49.4% TiO₂, was introduced into the reaction vessel. Six 10 mm diameter mild steel rods were
20 suspended in the reactor such that about 200 mm of the rods extended below the solution level. The mixture was allowed to react at 110° C for 3 hours, after which the temperature was allowed to fall steadily to 80°C over the next 3 hours. The resulting slurry was filtered through a
25 recessed plate filter and the cake was washed with fresh water. The filtrate contained 46 g/L Ti, 38 g/L Fe²⁺, 20 g/L Fe³⁺, 513 g/L free H₂SO₄, and had a specific gravity of 1.553 g/cm³. The weight of the washed filter cake was 86 kg with a moisture content of 26.2%. The washed filter
30 cake was assayed on a dry weight basis and was found to contain 13.3% FeO, 22.7% Fe₂O₃ and 49.7% TiO₂.

Based on the weights and compositions of the feed and product and cakes, 39.7% of the TiO₂ in the feed cake
35 dissolved during the leach process.

Example 3

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This example describes the reduction and removal of Fe^{3+} from the solution produced as described in Examples 1-2.

5

A 5 L baffled glass reactor fitted with an 80 mm Rushton 6 turbine agitator was filled with 4 L of a solution containing 13.2 g/L Fe^{3+} , 38.5 g/L Fe^{2+} , 505 g/L free H_2SO_4 and 40 g/L Ti. The agitation rate was set at 500 rpm. The reactor was temperature controlled to 50°C. On reaching this temperature a pump was used to recirculate the solution at 100 mL/min from the glass vessel, and through a 4 L fibre reinforced plastic (FRP) vessel containing a single 150 mm x 150 mm x 150 mm compressed bale of commercial detinned scrap steel. The solution was introduced to the bottom of the FRP vessel and flowed up through the scrap and overflowed via gravity back into the glass reactor. The bale of scrap was height adjusted to be fully submerged below the level of the solution in the FRP vessel. After recirculating the solution for 45 min it was found that all Fe^{3+} had been consumed. After 60 minutes the pump was turned off and the bale of scrap removed, whereupon it was found the solution contained 0 g/L Fe^{3+} , 93 g/L Fe^{2+} and 8.5 g/L Ti^{3+} .

25

Example 4

This example shows that ferrous sulfate may be batch precipitated from an ilmenite leach solution.

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An ilmenite leach solution containing 0.1 g/L Fe^{3+} , 98.2 g/L Fe^{2+} , 48 g/L Ti and 399 g/L free H_2SO_4 , prepared in the manner described in Example 3, was placed in a beaker and cooled overnight. Green ferrous sulfate heptahydrate crystals with composition 18.5% Fe, 10.5% S, 0.23% Ti and 0.15% Mn were then recovered from the resulting slurry. The filtrate was assayed and found to

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- 25 -

contain <1 g/L Fe^{3+} , 30.2 g/L Fe^{2+} and 539 g/L free H_2SO_4 .

Example 5

This example shows that titanyl sulfate dihydrate, $\text{TiOSO}_4 \cdot 2\text{H}_2\text{O}$, crystals may be batch precipitated from an ilmenite leach solution prepared in the manner of Examples 1-2 by the addition of sulfuric acid and that a high strength solution suitable for pigment manufacturing may be generated by dissolution of the crystals.

Sulfuric acid (98%, 450 g) was mixed with an ilmenite leach solution (1500 mL) containing 440 g/L free H_2SO_4 , 35.4 g/L Fe^{2+} , 7.4 g/L Fe^{3+} and 29 g/L Ti in a glass reactor equipped with baffles and a Teflon agitator. The resulting solution was heated to 110° C and titanyl sulfate crystals (4 g) were added as seed material. The mixture was stirred at this temperature for a total of 6 hours, during which a thick precipitate formed. The slurry was filtered and the cake was washed with water to give a wet filter cake (238 g). The filtrate contained 16 g/L Ti, 638 g/L H_2SO_4 and 48 g/L Fe, of which 6.6 g/L was as Fe^{3+} . The filter cake dissolved after 3 hours to produce a titanyl sulfate solution containing 160 g/L Ti and 8.3 g/L Fe.

Example 6

This example describes the continuous precipitation of titanyl sulfate dihydrate, $\text{TiOSO}_4 \cdot 2\text{H}_2\text{O}$, crystals, followed by vacuum filtration.

Ilmenite leach solution (603.6 L) prepared as described in Examples 1-2, containing 524.7 g/L free H_2SO_4 , 14.5 g/L Fe^{2+} , 4.3 g/L Fe^{3+} and 41.2 g/L Ti was mixed in an agitated fibreglass reactor with titanyl sulfate filtrate (1043.2 L) containing 637.5 g/L free H_2SO_4 , 44.7 g/L Fe^{2+} ,

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12.8 g/L Fe^{3+} and 6.1 g/L Ti. Sulfuric acid (98%, 88.3 L) was then added along with titanyl sulfate filter cake (10 kg, 14% w/w solids) and the temperature was raised to 110°C. The reactor was 1.35 m diameter, with 1.3 m solution depth and contained a draft tube to improve mixing and the uniformity of mixing inside the reactor with minimal power input. The draft tube was 0.9 m internal diameter, 0.87 m high and raised 0.25 m from the bottom of the reactor. The reactor was fitted with an axial turbine with diameter of 0.6 m and raised 0.5 m from the floor of the reactor. The turbine operated at 250 rpm. The reactor was allowed to stir at temperature for 12 hours and a sample was taken and filtered. The titanium concentration in the liquor had dropped from an initial combined level of 17.3 g/L to 9.0 g/L. The feed and product pumps were started and set to flowrates of 4.6 L/min to allow for a 4.9 hour residence time with a constant combined feed solution containing 17.5 g/L Ti and 660 g/L H_2SO_4 . The precipitator was run continuously this way for 10 hours producing 2742 L of titanyl sulfate slurry. Regular samples were taken from the reactor and filtered and analysed. These filtrate samples gave average concentrations of 7.5 g/L Ti and 611.8 g/L H_2SO_4 . The precipitated titanyl sulfate dihydrate was separated from the slurry using a belt filter, giving approximately 780 kg of filter cake with solids loading 14% w/w.

Example 7

This example demonstrates that titanyl sulfate dihydrate, $\text{TiOSO}_4 \cdot 2\text{H}_2\text{O}$, crystals prepared in the manner of Examples 5 and 6 may be dissolved in water to produce a high strength titanyl solution.

Titanyl sulfate dihydrate filter cake (19 kg) produced using the process described in Example 6 was repulped into a pumpable slurry using a solution containing

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400 g/L H_2SO_4 (4 L) mixed with re-pulp filtrate (36 L) containing 485 g/L free H_2SO_4 , 6.7 g/L Fe^{2+} , 9.6 g/L Fe^{3+} and 5.9 g/L Ti. The slurry was allowed to stir for 15 minutes and then was filtered using a plate and frame
5 filter. A sample of the filtrate from this filtering step was analysed and was found to contain 510 g/L free H_2SO_4 , 8.9 g/L Fe^{2+} , 10.7 g/L Fe^{3+} and 7.4 g/L Ti. Water (50 L) was pumped through the filter to wash the solids. A sample of the filtrate from the washing step was analysed
10 and found to contain 137 g/L free H_2SO_4 , 2.2 g/L Fe^{2+} , 3 g/L Fe^{3+} and 3.3 g/L Ti. The washed solids were collected and were allowed to dissolve overnight. The resulting titanyl sulfate solution was filtered to remove fine, undissolved solids, which were predominately silica.

15 The solution was found by assay to contain 467 g/L total H_2SO_4 , 1.7 g/L Fe^{2+} , 6.5 g/L Fe^{3+} and 194 g/L Ti.

20 Example 8

This example describes the conversion of the titanyl sulfate dihydrate filter cake into a titanium solution with higher than 200 g/L Ti which is suitable for production of pigment.

25 Recycled filtration liquor (60 kg) containing 378.1 g/L free H_2SO_4 , 12.8 g/L Fe^{2+} and 7.3 g/L Ti was mixed with recycled wash water (55 kg) containing 86.9 g/L free H_2SO_4 , 3.5 g/L Fe^{2+} and 3.6 g/L Ti and with 450 g/L sulfuric
30 acid (15.5 kg). This liquor was then used to re-pulp titanyl sulfate dihydrate filter cake (64 kg, 14% w/w solids) prepared as described in Example 6. The re-pulped slurry was filtered using a membrane pressure filter and was then washed with water (70 L). The washed cake was
35 squeezed at a pressure of 4 bar for 5 minutes and compressed air was then blown through the cake for a further 5 minutes. The filter cake was then removed from

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the filter and transferred to a container where it dissolved over a period of several hours to give a titanyl sulfate solution (6.5 kg) containing 254 g/L Ti and 523 g/L total H_2SO_4 .

5

Example 9

This example describes the conversion of a titanyl sulfate dihydrate slurry directly into a high concentration titanium solution suitable for production of pigment, without an intermediate re-pulp step.

Titanyl sulfate slurry (108 L) produced from the reactor described in Example 6 was filtered using a membrane pressure filter, instead of the belt filter described in Example 6. Recycled filter acid (45 L) containing 338.4 g/L free H_2SO_4 , 10.1 g/L Fe^{2+} , 2.3 g/L Fe^{3+} and 10.1 g/L Ti was mixed with recycled wash water (50 L) containing 93.2 g/L free H_2SO_4 , 3.4 g/L Fe^{2+} , 0.7 g/L Fe^{3+} and 3.4 g/L Ti and with 450 g/L sulfuric acid (10 L). This mixed acid stream was then passed through the membrane pressure filter to wash the filtered solids. The solids were then further washed with water (50 L) and squeezed at a pressure of 4 bar for 5 minutes. Compressed air was then blown through the washed cake for 5 minutes. The filter cake was then removed from the filter and transferred to a container where it dissolved over a period of several hours to give a titanyl sulfate solution containing 218 g/L Ti and 333.5 g/L free H_2SO_4 .

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Example 10

This example describes the precipitation of pigment capable titanium hydroxide from high strength titanyl sulfate solution, using conventional practice.

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High strength titanyl sulfate solution (2.5 L) prepared as described in Example 7 was filtered to remove residual solids, then zinc dust (13 g) was added with stirring to remove ferric ions and to generate trivalent titanium. The solution on analysis was found to contain approximately 3.0 g/L of Ti^{3+} . Concentrated sulfuric acid was added to give an A/T ratio of 1.70 ± 0.05 . The liquor was then concentrated by evaporation under reduced pressure to give a viscosity of 22-25 cp at $60^{\circ}C$ and 330 ± 10 g/L of TiO_2 in the final concentrated liquor.

Hydrolysis was carried out based on the Blumenfeld method. A water heel (0.5 L) was heated to $98 \pm 1^{\circ}C$ in a glass reactor equipped with external electrical heating, a temperature controller, thermocouple and a rake type stirrer. The pretreated A/T controlled liquor (2.0 L) was separately heated to $98 \pm 1^{\circ}C$ before being added to the water heel at a controlled rate such that all the liquor was added to the heel within 17 ± 1 minutes. The temperature profile was then controlled to precipitate TiO_2 at a relative rate of 0.7 to 1.0% per minute by ramping the heating rate to give a temperature rise $0.5^{\circ}C$ per min up to the boiling point. Agitation and heating were then stopped for 30 minutes. After this 'stop time' agitation and heating were reapplied to continue precipitation at the rate of 0.7 to 1.0% per minute relative to the initial TiO_2 concentration. After an overall reaction time of 5 hours the batch was quenched with 2 L of water. Once the solution was cooled to less than $60^{\circ}C$ the solution was vacuum filtered using a Buchner funnel and the precipitate washed with water (6 L) at $60^{\circ}C$. The cake was allowed to dry by filtration to achieve 30% solids as TiO_2 . In total 608 g of titanium hydroxide was produced, corresponding to a yield of 96%.

Example 11

- 30 -

This example describes the production of rutile seed slurry, which may be used to assist with the rutilisation process during calcination.

5 Titanium hydroxide filter cake (750 g, loss on ignition 68%) prepared as described in Example 10 was placed in a reaction vessel equipped with agitation and external heating. To the paste, pellets of sodium hydroxide (495 g) were slowly added over 30 minutes. A
10 lid was then placed over the vessel. The temperature was set to 126°C and was maintained at this level with agitation for a further 60 minutes. At the end of this time the reaction was quenched to 60° C by adding sufficient water to lower the solids loading to 140 g/L
15 equivalent TiO₂ (resulting in a total slurry volume of 1713 mL). The slurry was then filtered using a Buchner funnel, and the precipitate washed with water at 60° C until the wash filtrate contained approximately 1 g/L equivalent Na₂O, measured using a calibrated conductivity meter.

20

The washed filter cake was then transferred to a reflux vessel equipped with an agitator and reslurried to 255 g/L equivalent TiO₂ (giving a slurry volume of 941 mL). The slurry pH was adjusted to 2.8 using concentrated HCl
25 (90 mL, 33% w/v). A 1 g sample was removed to test for cake quality. To the remaining slurry sufficient concentrated HCl (298 mL, 33% w/v) was added to give an HCl:TiO₂ ratio of 0.41, and the temperature was raised to 60° C. The temperature was then increased to the boiling
30 point at a controlled rate of 1° C per minute, and maintained at the boiling point for 90 minutes, after which the slurry was quenched with water to a volume of 2400 mL, giving a solids loading equivalent to 97 g/L TiO₂. A small sample was neutralized with NaOH, filtered, washed
35 and dried was found by XRD to contain 100% rutile form TiO(OH)₂.

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Example 12

This example describes conventional reductive acid leaching of precipitated titanium hydroxide to remove chromophores.

The filtered cake (63.5 g) from Example 10 was slurried in water (0.07 L) in a glass vessel equipped with a laboratory agitator. Concentrated H_2SO_4 (98%, 9.0 g) was added to the stirred slurry after which coarse rutile nuclei (8.6 mL; prepared as described in Example 11) was added to the slurry to achieve 4% added rutile TiO_2 . The seeded slurry was made up to 0.1 L with water and heated to 75° C. Once at temperature zinc dust was added (0.5 g) and the slurry was maintained at temperature for 2 hours. The slurry was then cooled to 60° C and vacuum filtered in a Buchner funnel. The final filtrate was analysed for Ti^{3+} concentration to confirm sufficient Ti^{3+} was present (>0.4 g/L Ti^{3+} preferred (as TiO_2)). The cake was then washed with water at 60° C (three times the volume of precipitate cake). The final cake (60 g) was allowed to dry under vacuum filtration to approximately 30% solids.

Example 13

This example describes calcination of titanium hydroxide to produce a substantially rutilised TiO_2 calcine with crystal size suitable for pigment production.

The cake paste (300 g) prepared as described in Example 12 was mechanically mixed in the presence of H_3PO_4 (98% solution), $\text{Al}_2(\text{SO}_4)_3$, K_2SO_4 to give 0.15% P_2O_5 , 0.18% Al_2O_3 and 0.28% K_2O as calculated after calcination, until a homogenous mixture is obtained. The paste was the extruded through a 5 mm die onto glass surface, covered then dried in a 75° C laboratory oven for 12 hours. The solids were then transferred to an electrically heated

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muffle furnace and the temperature was ramped to 920° C for 3 hours. The calcined solids were removed from the furnace and allowed to cool to ambient temperature, and the rutilisation measured by XRD was found to be 97.3%.

5

Example 14

Cooled TiO₂ solids (800 g) prepared as described in Example 13 were then processed through a laboratory
10 hammer mill and sieved to achieve a particle size of less than 90 microns. The milled particles were then slurried in room temperature water to give a solids loading of 400 g/L (as TiO₂) with the aid of organic dispersant (1,1,1-tris-hydroxymethyl propane). The dispersed slurry was pH
15 adjusted to 10-11 by the addition of 10% w/v NaOH solution. The slurry was then passed through a hydraulic bead mill (bead size 0.8-1.0 mm, zirconia stabilized) in recirculation mode until a mean particle size of 0.27 µm was achieved. The slurry was then passed through a 325 µm
20 sieve and the oversize was discarded.

The sieved slurry (2 L) was then transferred to a 3 L beaker and heated to 50° C using an external electric heating mantle. Four solutions (20% w/v H₂SO₄, 10% w/v
25 NaOH, 100 g/L (as ZrO₂) ZrCl₂.8H₂O and NaAlO₂ (caustic stabilized solution containing 17-18% w/w Al₂O₃)) were filled into separate 50 ml burettes and their volumes noted. The reagents were added at temperature such that a final concentration of Al₂O₃ (3.5% of TiO₂ content) and ZrO₂
30 (0.88% of TiO₂ content) was achieved. The slurry was then filtered and washed with water at 60° C to achieve soluble salts in the cake as less than 0.1% as Na₂SO₄, and dried for about 3 hours under vacuum. The cake paste was then mechanically mixed in the presence of organic dispersant
35 to achieve 0.2% carbon (w/w) on the TiO₂. The paste was then extruded through a 5 mm die onto glass surface, which was covered and dried in a 75° C laboratory oven for 6

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hours to achieve less than 1.0% H₂O. The solids were then lightly hammer milled and the resulting solids passed through a laboratory air microniser which was operated at 6 bar (dried compressed air) for injection and grinding. The micronised product mean particle size was milled to between 0.30 and 0.33 μ m as determined by optical density measurements.

Example 15

This example shows the ability to continuously hydrolyse high strength titanium solution to produce coarse TiO(OH)₂ which may be settled and filtered readily.

A continuous pilot plant comprising of 2 x 5 L fibre-reinforced plastic (FRP) vessels, equipped with axial turbines and heaters, and an FRP thickener of diameter 30 cm and height 90 cm, equipped with rakes and a rake drive motor, was assembled. The FRP vessels and thickener were arranged in series with cascading overflow pipes between them to allow slurry to flow from vessel to vessel by gravity. An acidic slurry of titanium hydroxide (4 kg) prepared as described in Example 10 was placed in the first vessel as seed, and a solution of 300 g/L of H₂SO₄ in water (5 L) was placed in the second vessel to assist the initial start up phase. The vessels were heated to a temperature of 100° C with stirring. On reaching temperature a solution of titanium sulfate prepared as described in Example 7, and containing Ti 130 g/L, Ti³⁺ 5 g/L, total acid 330 g/L and Fe 10 g/L, was pumped to the first vessel at a rate of 7.5 mL/min. Water was also added at a rate of 6 mL/min to correct for evaporation. On filling of the thickener, a portion of the underflow corresponding to 5 mL/min and 20% w/w solids loading was thereafter continuously pumped to the first vessel to act as seed. In total the hydrolysis pilot plant was operated continuously for 75 hours. On reaching

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steady state under these process conditions it was found that the vessels and process streams equilibrated to the following compositions.

	Ti g/L	Ti ³⁺ g/L	Fe g/L
Feed solution	130	5	10
Vessel 1	70	1.4	11
Vessel 2	14	0.9	9

5

Combined thickener underflow flowrate was 7 mL min (of which 5 mL/min was recycled as described).

Equilibrated thickener overflow flowrate was 9 mL/min.

The solids loading in the thickener underflow reached 30%

10 w/w by the end of the run. The particle size of the thickener underflow solids was determined using a Malvern 2000 laser sizer and was found to be d_{50} 7.8 μm .

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CLAIMS

1. A sulfate process for producing titania from a titaniferous material (such as ilmenite) of the type which
5 includes the steps of:

(a) leaching the solid titaniferous material with a leach solution containing sulfuric acid and forming a process solution that includes an acidic solution of
10 titanyl sulfate (TiOSO_4) and iron sulfate (FeSO_4);

(b) separating the process solution and a residual solid phase from the leach step (a);

15 (c) precipitating titanyl sulfate from the process solution from step (b);

(d) separating the precipitated titanyl sulfate from the process solution;
20

(e) treating the precipitated titanyl sulfate and producing a solution containing titanyl sulfate;

(f) hydrolysing the titanyl sulfate in the
25 solution and forming a solid phase containing hydrated titanium oxides and a liquid phase;

(g) separating the solid phase containing hydrated titanium oxides and the liquid phase;
30

(h) calcining the solid phase from step (g) and forming titania; and

(i) removing iron sulfate from the process
35 solution from step (b) and/or the depleted process solution from step (d).

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2. The process defined in claim 1 further includes supplying the separated process solution from step (d) and/or the separated liquid phase from step (g) to leach step (a).

5

3. The process defined in claim 1 or claim 2 wherein step (d) includes separating the precipitated titanyl sulfate from the process solution from step (c) by filtering the process solution from step (c) using a filter, such as a pressure filter, and forming a filter cake and a filtrate.

10

4. The process defined in claim 3 wherein step (d) includes washing the filter cake with fresh acid and/or recycled acid, for example from the hydrolysis step (f), to displace entrained solution contain impurities and thereby improving purity of the high strength Ti solution for the hydrolysis step (f).

15

5. The process defined in claim 3 or claim 4 wherein the filtrate from the filter contains 700 g/L sulfuric acid (50% w/v), 10 g/L titanium and 40 g/L iron in solution and the process includes supplying the filtrate to the leach step (a).

20

25

6. The process defined in any one of claims 3 to 5 includes re-pulping the filter cake and forming an acidic slurry of titanyl sulfate and thereafter filtering the slurry and washing the filter cake.

30

7. The process defined in claim 6 includes re-pulping the filter cake with an acidic solution in order to retain high acidity in the resultant slurry and so as to form an acidic slurry that has a low solids loading, typically less than 10% by weight.

35

8. The process defined in claim 7 wherein the

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acidity of the acidic solution is at least 300 g/L.

9. The process defined in claim 7 wherein the acidity of the acidic solution is of the order of 400 g/L.

10. The process defined in any one of claims 7 to 9 wherein the acidic solution includes the liquid phase recovered from the hydrolysis step (f) and/or recycled re-pulp acid.

11. The process defined in any one of claims 6 to 10 includes re-pulping the filter cake under agitated conditions.

12. The process defined in any one of claims 7 to 11 includes filtering the acidic slurry using a filter, such as a pressure filter, for example a pressure belt filter, and forming an acidic filter cake of titanyl sulfate and a filtrate.

13. The process defined in claim 12 includes washing the acidic filter cake with water and reducing the acidity of the liquid component of the filter cake to be less than 200 g/L acid.

14. The process defined in claims 12 or 13 wherein step (d) includes reducing the acidity of the liquid component of the filter cake and acidic minimising the retained water with acidic filter cake by washing the acidic filter cake with water under pressure filtration conditions, such as on a belt pressure filter.

15. The process defined in any one of the preceding claims wherein step (d) includes minimizing the amount of water that is retained with the precipitated titanyl sulfate to maximise the titanium concentration in the subsequently dissolved process solution produced in step

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(e).

16. The process defined in claim 15 wherein step (d) includes minimizing the amount of water that is retained with the precipitated titanyl sulfate to maximise the titanium concentration in the subsequently dissolved liquor produced in step (e) to concentrations of at least 150 g/L, more preferably at least 200 g/L titanium.

17. The process defined in claim 14 or claim 16 wherein step (d) includes minimising the retained water by evaporating or other suitable concentration options for removing retained water.

18. The process defined in claim 13 or claim 14 wherein step (e) includes transferring the washed filter cake to a stirred tank and allowing the cake to dissolve to a process solution containing a high concentration of titanium, preferably at least 150 g/L, more preferably at least 200 g/L titanium.

19. The process defined in claim 18 includes heating the washed filter cake in the stirred tank, preferably to a temperature of the order of 60°C in order to speed up the dissolution process.

20. The process defined in claim 18 or claim 19 includes carrying out step (e) on a batch or a continuous basis.

21. The process defined in claim 20 includes recycling high strength process solution ("rich liquor") produced in the stirred tank to the tank to improve agitation and/or handling of the slurry as dissolution is proceeding.

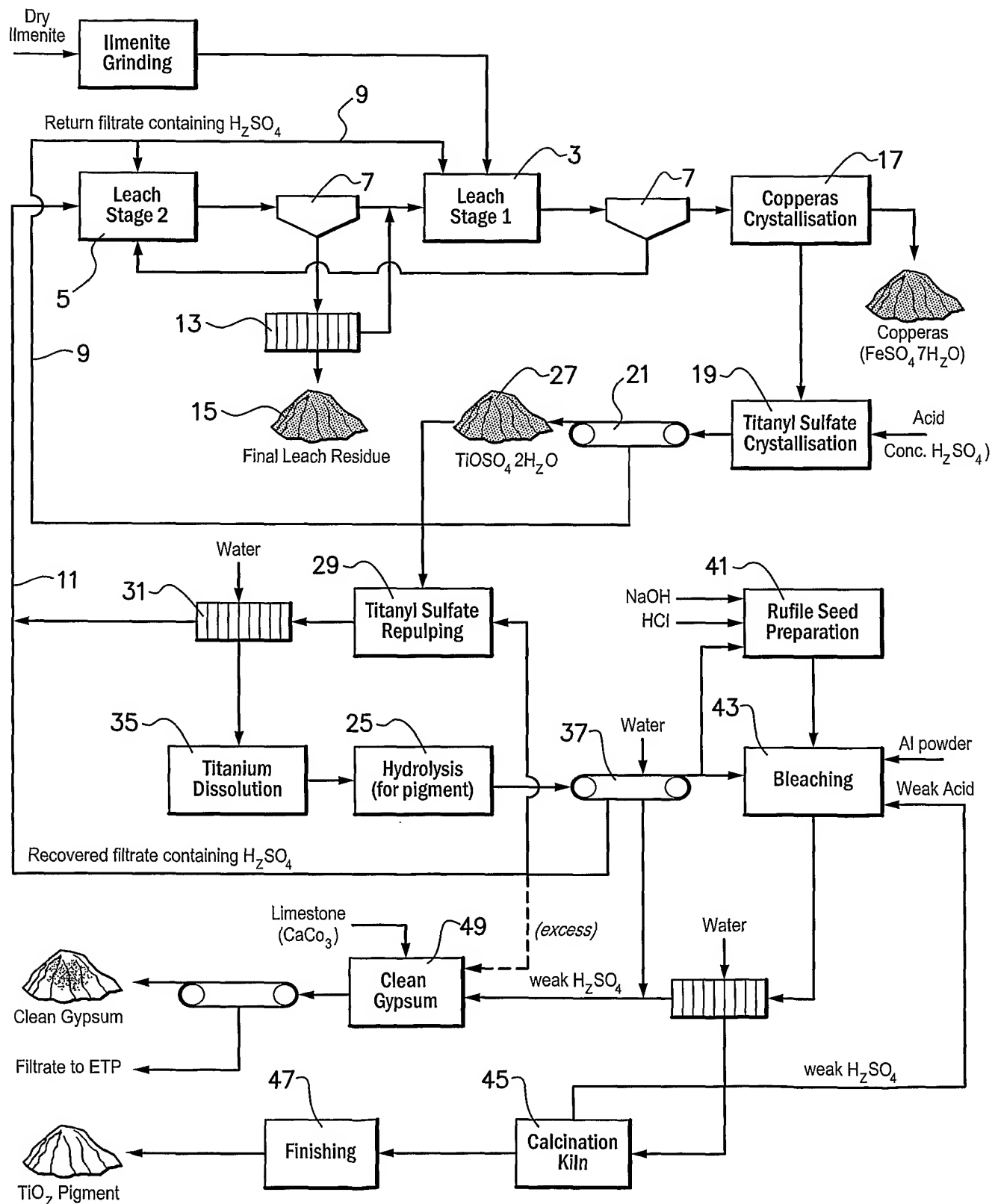
22. The process defined in claim 1 or claim 2 wherein

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steps (d) and (e) are carried out successively, with no separation of an intermediate solid product.

23. The process defined in claim 22 wherein steps (d)
5 and (e) include separating the precipitated titanyl
sulfate from the process solution from step (c), for
example on a filter and producing a filter cake, and
thereafter directly washing the filter cake with the
liquid phase from hydrolysis step (f) and/or water, for
10 example while the filter cake is on the filter.

24. The process defined in claim 23 wherein steps (d)
and (e) include air blowing and/or squeezing the filter
cake removing additional liquid from the filter cake and
15 produce a high Ti concentration in the subsequent
dissolved liquor.



INTERNATIONAL SEARCH REPORT

International application No.

PCT/AU2006/000468

A. CLASSIFICATION OF SUBJECT MATTER

Int. Cl.

C22B 3/08 (2006.01)

C01G 23/047 (2006.01)

C22B 3/44 (2006.01)

C01G 23/00 (2006.01)

C22B 3/00 (2006.01)

C22B 34/12 (2006.01)

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

WPAT; JAPIO; USPTO; Espace@net; IPC (above) and Keywords - titani+, TiO2+, titanyl+, ilmenite+, rutil+, leach+, precipitat+, sul??ric acid, sul??ate+, process+

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P,X	WO 2005/038060 A (BHP BILLITON INNOVATION PTY LTD), 28 April 2005 Whole document	1-4 & 6-21
X,Y	WO 2004/035841 A (BHP BILLITON INNOVATION PTY LTD), 29 April 2004 Whole document	1-3 & 15
X,Y	WO 2004/035842 A (BHP BILLITON INNOVATION PTY LTD), 29 April 2004 Whole document	1-3 & 15



Further documents are listed in the continuation of Box C



See patent family annex

* Special categories of cited documents:	
"A" document defining the general state of the art which is not considered to be of particular relevance	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"E" earlier application or patent but published on or after the international filing date	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"O" document referring to an oral disclosure, use, exhibition or other means	"&" document member of the same patent family
"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search
10 May 2006Date of mailing of the international search report
22 MAY 2006

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INTERNATIONAL SEARCH REPORT

International application No.

PCT/AU2006/000468

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X,Y	WO 2004/035843 A (BHP BILLITON INNOVATION PTY LTD), 29 April 2004 Whole document	1-3 & 15
Y	CA 2431257 A (ROSSMALI TECHNOLOGY HOLDINGS PTY LTD [ZA]), 20 June 2002 Whole document	1-3 & 15
A	US 4288415 A (RAHM et al), 8 September 1981 Whole document	1-25
A	US 4288416 A (DAVIS et al), 8 September 1981 Whole document	1-25

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No.

PCT/AU2006/000468

This Annex lists the known "A" publication level patent family members relating to the patent documents cited in the above-mentioned international search report. The Australian Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

Patent Document Cited in Search Report		Patent Family Member					
WO	2005038060	US	2005180903				
WO	2004035841	AU	2003271423	BR	0315412	CN	1729304
		EP	1558771	RU	2005115123		
WO	2004035842	AU	2003271424	BR	0315409	CN	1729305
		EP	1558772	RU	2005115130		
WO	2004035843	AU	2003271425	CN	1729303	EP	1563107
		RU	2005115122				
US	4288416	AU	60677/80	BE	886327	BR	8004975
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		GB	2055781	IN	154400	JP	56037220
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		CA	1157229	DE	3030178	ES	8106468
		FI	802511	FI	831931	FR	2463100
		IN	154398	JP	56037219	KR	8302446
		NL	8004489	NO	802361	PL	226165
		US	4288417	YU	191080	YU	287082
		ZA	8004804				
CA	2431257	AU	62583/01	BR	0116677	WO	0248412
		CN	1479795	EP	1341939	US	2004136899
		ZA	200104774				
Due to data integration issues this family listing may not include 10 digit Australian applications filed since May 2001.							
END OF ANNEX							